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(71) Applicant (for all designated States except US): UHDE GMBH [DE/DE]; Friedrich-Uhde-Strasse 15, 44141 Dortmund (DE).

(72) Inventors; and

(75) Inventors/Applicants (US only): SCHWEFER, Meinhard [DE/DE]; Aufm Ufer 12, 59872 Meschede (DE). GROVES, Michael [GB/DE]; Isenberger Weg 12, 45529 Hattingen (DE).

(74) Attorney: ACKERMANN, Joachim; Postfach 11 13 26, 60048 Frankfurt (DE).

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(54) Title: DENITRIFICATION METHOD

(54) Bezeichnung: ENTSTICKUNGSVERFAHREN

**WO 03/084646 A1** (57) **Abstract:** Disclosed is a method for reducing the content of NO<sub>x</sub> and N<sub>2</sub>O in gases, especially in process gases and off gases, comprising the following steps: a) at least one reducing agent containing nitrogen is added to the gas containing NO<sub>x</sub> and N<sub>2</sub>O in an amount required for at least full reduction of the NO<sub>x</sub>; b) a hydrocarbon from carbon monoxide, hydrogen or a mixture of one or several of said gases is added to the gas containing NO<sub>x</sub> and N<sub>2</sub>O for the reduction the N<sub>2</sub>O; and c) the gas mixture is guided into at least one reaction zone with temperatures of up to 450 °C, containing one or several zeolites loaded with iron. The method can especially be used in the production of nitre in off gases from power plants or in gas turbines.

(57) **Zusammenfassung:** Beschrieben wird ein Verfahren zur Minderung des Gehalts von NO<sub>x</sub> und N<sub>2</sub>O in Gasen, insbesondere in Prozessgasen und Abgasen, umfassend die Massnahmen: a) Zugabe mindestens eines Stickstoff enthaltenden Reduktionsmittels zu dem NO<sub>x</sub> und N<sub>2</sub>O enthaltenden Gas in einer solchen Menge, wie mindestens zur vollständigen Reduktion des NO<sub>x</sub> benötigt wird, b) Zugabe eines Kohlenwasserstoffes, von Kohlenmonoxid, von Wasserstoff oder von einem Gemisch einer oder mehrerer dieser Gase zu dem NO<sub>x</sub> und N<sub>2</sub>O enthaltenden Gas für die Reduktion des N<sub>2</sub>O, und c) Leiten des Gasgemisches in mindestens eine Reaktionszone mit Temperaturen von bis zu 450 °C, die einen oder mehrere mit Eisen beladene Zeolithe enthält. Das Verfahren lässt sich insbesondere bei der Salpetersäureproduktion, bei Kraftwerksabgasen oder bei Gasturbinen einsetzen.

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**PROCESS FOR THE REMOVAL OF NITROGEN OXIDES**

Meinhard Schwefer

and

Michael Groves

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202ku05.us (9600\*23)

DeNO<sub>x</sub> process

The invention relates to a process for reducing the content of nitrogen oxides in offgases or process 5 gases.

In many processes, e.g. combustion processes or the industrial preparation of nitric acid, an offgas laden with nitrogen monoxide NO, nitrogen dioxide NO<sub>2</sub> 10 (together referred to as NO<sub>x</sub>) and also nitrous oxide N<sub>2</sub>O is formed. While NO and NO<sub>2</sub> have long been known as compounds having ecotoxicologically relevance (acid rain, smog formation) and are subjected worldwide to limits for their maximum permissible emissions, nitrous oxide 15 has in recent years also increasingly moved into the focus of environmental protection, since it contributes to a not inconsiderable extent to the degradation of stratospheric ozone and to the greenhouse effect. There is thus, for reasons of environmental protection, an 20 urgent need for technical solutions which enable nitrous oxide emissions to be eliminated together with the NO<sub>x</sub> emissions.

There are numerous possible ways of removing N<sub>2</sub>O and NO<sub>x</sub> 25 separately, and these can be combined in an appropriate way in two-stage processes.

It is known from EP-A-393,917 that nitrogen oxides can be removed from gases by means of ammonia and selected 30 zeolite catalysts. However, this document describes only the reduction of NO<sub>x</sub> by means of ammonia. Zeolites proposed are the types USY, beta and ZSM-20, which have large pores and a specific silicon dioxide:aluminum oxide ratio.

35

It is known from Chem. Commun. 2000, 745-6 that N<sub>2</sub>O can be selectively reduced catalytically by means of methane in the presence of excess oxygen and the

- 2 -

presence of an iron-laden zeolite of the beta type (BEA).

JP-A-09/000,884 discloses a process for reducing the  
5 content of N<sub>2</sub>O and NO, in which ammonia, alcohols and/or hydrocarbons are used as reducing agent and zeolites of the pentasil or mordenite type are used as catalyst.

10 Starting out from this prior art, the present invention provides a simple but extremely economical process which gives excellent conversions both for the removal of NO<sub>x</sub> and for the removal of N<sub>2</sub>O at low operating temperatures.

15 It has surprisingly been found that in the reduction of N<sub>2</sub>O from NO<sub>x</sub>-containing gases, the NO<sub>x</sub> has an inhibiting effect on the removal of N<sub>2</sub>O and that improved reduction of N<sub>2</sub>O occurs when the NO<sub>x</sub> is completely  
20 reduced.

25 The invention provides a process for reducing the content of NO<sub>x</sub> and N<sub>2</sub>O in gases, in particular in process gases and offgases, which comprises the measures:

- a) addition of at least one nitrogen-containing reducing agent, in particular ammonia, to the NO<sub>x</sub>- and N<sub>2</sub>O-containing gas in at least the amount required for complete reduction of the NO<sub>x</sub>,
- 30 b) addition of a hydrocarbon, of carbon monoxide, of hydrogen or of a mixture of a plurality of these gases to the NO<sub>x</sub>- and N<sub>2</sub>O-containing gas for the reduction of the N<sub>2</sub>O and
- c) introduction of the gas mixture into at least one  
35 reaction zone at temperatures of up to 450°C which contains one or more iron-laden zeolites, preferably iron-laden zeolites containing channels made up of twelve-membered rings, in particular

- 3 -

iron-laden zeolites all of whose channels are made up of twelve-membered rings, very particularly preferably iron-laden zeolites of the BEA or FAU type.

5

To carry out the process of the invention, the  $N_2O$ - and  $NO_x$ -containing gas is firstly mixed with a nitrogen-containing reducing agent and hydrocarbons or carbon monoxide and/or hydrogen and subsequently passed over 10 the iron-laden zeolite(s) at a temperature of less than 450°C to remove  $N_2O$  and  $NO_x$ , in each case by reduction.

According to feature a) of the process of the invention, the nitrogen-containing reducing agent is 15 added in at least the amount required for complete reduction of the  $NO_x$ . For the purposes of the present description, the amount of nitrogen-containing reducing agent required for complete reduction of the  $NO_x$  is that amount of nitrogen-containing reducing agent which 20 is necessary to reduce the proportion of  $NO_x$  in the gas mixture to a residual content of less than 10 ppm, preferably less than 5 ppm and in particular less than 1 ppm.

25 As nitrogen-containing reducing agents, it is possible to employ any compounds which are capable of reducing  $NO_x$ . Examples of such reducing agents are hydrogen compounds of nitrogen, e.g. azanes, hydroxyl derivatives of azanes and also amines, oximes, 30 carbamates, urea or urea derivatives.

Examples of azanes are hydrazine and in particular ammonia.

35 An example of a hydroxyl derivative of azanes is hydroxylamine.

Examples of amines are primary aliphatic amines such as

methylamine.

An example of a carbamate is ammonium carbamate.

5 Examples of urea derivatives are N,N'-substituted ureas such as N,N'-dimethyl urea. Ureas and urea derivatives are preferably used in the form of aqueous solutions.

10 According to feature b) of the process of the invention, the hydrocarbon, the carbon monoxide and/or the hydrogen are added to reduce the N<sub>2</sub>O. These reducing agents are added in the amount required for the reduction of the N<sub>2</sub>O. For the purposes of the present description, this means that amount of reducing 15 agent which is necessary to reduce the N<sub>2</sub>O in the gas mixture either completely or to a desired final concentration.

20 In general, the temperature in the reaction zone is from 200 to 450°C, preferably from 250 to 450°C.

25 The reduction of the content of NO<sub>x</sub> and N<sub>2</sub>O is preferably effected in the presence of a single catalyst which consists essentially of one or more iron-laden zeolites.

30 When more than one and different zeolite catalysts are used, these can be mixed with one another or arranged in series. The latter arrangement is particularly advantageous when the zeolite closest to the inlet catalyzes especially the NO<sub>x</sub> reduction by means of a nitrogen-containing reducing agent and/or the zeolite closest to the outlet catalyzes especially the N<sub>2</sub>O reduction.

35

In this way, the NO<sub>x</sub> content in the first zeolite zone can be reduced particularly quickly and completely, so that the subsequent zeolite can fully fulfill its

- 5 -

function of reducing the N<sub>2</sub>O, since the NO<sub>x</sub> which has an adverse effect on the N<sub>2</sub>O reduction has been completely removed before entry into the second zone.

5 Reducing agents used for the purposes of the invention for the NO<sub>x</sub> are nitrogen-containing reducing agents, in particular ammonia, and those used for the N<sub>2</sub>O are hydrocarbons, hydrogen, carbon monoxide or mixtures thereof, e.g. synthesis gas.

10

The amount of reducing agent added to reduce the N<sub>2</sub>O depends essentially on the desired degree of removal of the N<sub>2</sub>O and on the type of reducing agent used. When hydrocarbons such as methane or propane are used, the 15 required amount is about 0.2 - 1 mol of hydrocarbon/1 mol of N<sub>2</sub>O to be reduced. Preference is given to amounts of 0.2 - 0.7 mol of hydrocarbon/1 mol of N<sub>2</sub>O to be reduced, in particular 0.2 - 0.5 mol of hydrocarbon/1 mol of N<sub>2</sub>O to be reduced.

20

This amount is very small compared with other values reported in the literature (cf., for example, figure 4 in JP-A-90/00,884). The fact that a high degree of removal of N<sub>2</sub>O is nevertheless achieved can be 25 explained by the complete reduction of NO<sub>x</sub>, as provided for according to the invention. This is a great advantage of the process of the invention since, in particular at high degrees of removal of N<sub>2</sub>O, the economics of the process are sensitive to the costs of 30 the reducing agent added.

Of course, what has been said regarding the amounts of the reducing agents used applies only to the case where the reduction of the nitrogen oxides to be removed is 35 subject to no other constraints, for example kinetic constraints. Such constraints are known to those skilled in the art. Thus, a given redox reaction always requires a certain minimum temperature and minimum

- 6 -

residence time in the reactor bed. Thus, the reduction of  $\text{NO}_x$  by means of  $\text{NH}_3$  proceeds so quickly that the kinetic constraints of the reaction have been overcome even for high space velocities ( $> 50\ 000\ \text{h}^{-1}$ ) at 5 temperatures as low as  $200^\circ\text{C}$ , while the reduction of  $\text{N}_2\text{O}$ , e.g. using methane, proceeds to completion only at significantly higher temperatures ( $> 300^\circ\text{C}$ ) and lower space velocities (about  $10\ 000\ \text{h}^{-1}$ ).

10 However, there is also an upper limit to the temperature in the process of the invention. Thus excessively high temperatures ( $> 450^\circ\text{C}$ ) effect a partial oxidation of the reducing agent added by means 15 of oxygen present in the offgas, so that this is no longer available for reducing the  $\text{NO}_x$  and  $\text{N}_2\text{O}$ . This applies particularly to the nitrogen-containing reducing agent added. The reduction of  $\text{NO}_x$  is then no longer complete, which results in the  $\text{N}_2\text{O}$  reduction also being inhibited.

20 .

Particularly preferred reducing agents for  $\text{N}_2\text{O}$  are saturated hydrocarbons or mixtures thereof, e.g. methane, ethane, propane, butane, synthesis gas or LPG.

25 Very particular preference is given to methane. This is used, in particular, in combination with an iron-laden zeolite of the BEA type.

30 The amount of nitrogen-containing reducing agent added has to be selected so as to be sufficient for complete reduction of the  $\text{NO}_x$ . In the case of ammonia, the stoichiometrically required amount for complete removal of the  $\text{NO}_x$  is 1.33 (8/6) mol of ammonia per one mol of  $\text{NO}_x$ . It has been found that when the pressure increases 35 or the reaction temperatures decrease, the amount of ammonia required for complete removal of the  $\text{NO}_x$  drops from the abovementioned 1.33 mol to 0.9 mol. A smaller proportion of ammonia may also be consumed in the  $\text{N}_2\text{O}$

- 7 -

reduction, so that sometimes a correspondingly larger amount of ammonia has to be used for the complete reduction of  $\text{NO}_x$ , for example up to 1.5 mol of ammonia per one mol of  $\text{NO}_x$ .

5

Catalysts used are the above-defined iron-laden zeolites or mixtures of iron-laden zeolites.

10 It has surprisingly been found that a very efficient reduction of  $\text{N}_2\text{O}$  can be carried out by means of such catalysts when the  $\text{NO}_x$  has been reduced completely.

15 Under the process conditions described here, the nitrogen-containing reducing agent acts mainly as a reducing agent for  $\text{NO}_x$  and the hydrocarbons, carbon monoxide and/or hydrogen act selectively to reduce the  $\text{N}_2\text{O}$  present in the gas.

20 The configuration of the reaction zone can be chosen freely for the purposes of the invention. It can, for example, be located in a tube reactor or radial basket reactor. The way in which the gaseous reducing agents are introduced into the gas stream to be treated can also be chosen freely for the purposes of the invention, as long as this is in the flow direction upstream of the reaction zone. It can be effected, for example, in the inward line upstream of the container for the catalyst bed or just before the bed. The reducing agents can be introduced in the form of gases 25 or in the form of a liquid or aqueous solution which vaporizes in the gas stream to be treated.

30 The order of addition of the reducing agents for  $\text{NO}_x$  and for  $\text{N}_2\text{O}$  can be chosen freely. Thus, the order of 35 the steps a) and b) can be exchanged or both types of reducing agent can be introduced in one step.

The catalysts used for the purposes of the invention

are known to those skilled in the art and can contain additives known per se, e.g. binders.

5 A catalyst or a catalyst component for the oxidation of any unreacted or partially oxidized material from the group consisting of one or more hydrocarbons, preferably CH<sub>4</sub> or C<sub>3</sub>H<sub>8</sub>, and also CO and H<sub>2</sub> can be integrated into the catalyst or located downstream thereof or connected to it in another way.

10 Catalysts used according to the invention are preferably based on zeolites into which iron has been introduced by means of solid-state ion exchange. For this purpose, it is usual to start out from 15 commercially available ammonium zeolites and the appropriate iron salts (e.g. FeSO<sub>4</sub> × 7 H<sub>2</sub>O) and mix these intensively with one another by mechanical means in a ball mill at room temperature. (Turek et al.; Appl. Catal. 184, (1999) 249-256; EP-A-0 955 080). 20 These publications are hereby expressly incorporated by reference. The catalyst powders obtained are subsequently calcined in air at temperatures in the range from 400 to 600°C in a muffle furnace. After calcination, the iron-containing zeolites are 25 intensively washed in distilled water and filtered off and dried. The iron-containing zeolites obtained in this way are finally treated with the appropriate binders and mixed and, for example, extruded to form cylindrical catalysts bodies. Suitable binders are all 30 binders customarily used; the most frequently used of these are aluminum silicates such as kaolin.

According to the present invention, the zeolites which can be used are laden with iron. The iron content based 35 on the mass of zeolite can be up to 25%, but is preferably from 0.1 to 10% (iron calculated as Fe<sub>2</sub>O<sub>3</sub>).

Precise details on the make-up or structure of these

- 9 -

zeolites are given in the Atlas of Zeolite Structure Types, Elsevier, 4<sup>th</sup> revised Edition 1996, which is hereby expressly incorporated by reference.

5 Zeolites which are particularly preferred according to the invention are of the FAU type and in particular of the BEA type.

10 The gas laden with nitrogen oxides is usually passed over the catalyst at a space velocity of from 200 to 200 000 h<sup>-1</sup>, preferably from 5000 to 100 000 h<sup>-1</sup>, based on the catalyst volume.

15 Here, the space velocity is the volume of gas mixture per hour divided by the volume of catalyst. The space velocity can thus be adjusted via the flow rate of the gas and/or via the amount of catalyst.

20 The process of the invention is generally carried out at a pressure in the range from 1 to 50 bar, preferably from 1 to 25 bar, with a higher operating pressure reducing the consumption of reducing agents, by-product formation and the leakage.

25 The introduction of the reducing agent into the gas to be treated is effected by means of a suitable apparatus, e.g. an appropriate pressure valve or appropriately configured nozzles.

30 The water content of the reaction gas is preferably in the range of < 25% by volume, in particular in the range < 15% by volume.

35 In general, a relatively low water concentration is preferred, since higher water contents would make higher operating temperatures necessary. This could, depending on the zeolite type used and the period of operation, exceed the hydrothermal stability limits of

- 10 -

the catalyst and thus has to be matched to the individual case chosen.

5 The presence of CO<sub>2</sub> and of other deactivating constituents of the reaction gas known to those skilled in the art should also be minimized where possible, since these would have adverse effects on the removal of N<sub>2</sub>O and NO<sub>x</sub>.

10 The process of the invention also operates in the presence of O<sub>2</sub>, since the catalysts used according to the invention have appropriate selectivities which at temperatures of < 450°C suppress reaction of the gaseous reducing agent, e.g. NH<sub>3</sub>, with O<sub>2</sub>.

15 All these influencing factors and also the chosen space velocity over the catalyst have to be taken into account in choosing the appropriate operating temperature of the reaction zone.

20 The conversions of N<sub>2</sub>O and NO<sub>x</sub> which can be achieved using the present process at low operating temperatures are virtually 100% for NO<sub>x</sub> and preferably > 70%, in particular > 80%, for N<sub>2</sub>O. The process is thus superior 25 to the prior art in terms of its performance, i.e. the achievable conversions of N<sub>2</sub>O and NO<sub>x</sub>, and in respect of the operating and capital costs.

30 As a result of the virtually complete reduction of NO<sub>x</sub>, a particularly high degree of removal of N<sub>2</sub>O is also achieved and a surprisingly low consumption of the reducing agent for N<sub>2</sub>O is achieved, which is an advantage of the invention.

35 The process of the invention can be employed, in particular, in nitric acid production, for offgases from power stations or for gas turbines. Process gases and offgases containing nitrogen oxides are obtained in

- 11 -

these processes, and the nitrogen oxides can be removed inexpensively from these gases by means of the process described here.

5 In one embodiment of the process of the invention, a mixture of CH<sub>4</sub> and NH<sub>3</sub> is mixed into a gas comprising nitrogen oxides and the two are fed together into a reactor containing an iron-laden zeolite of the BEA type and subjected to nitrogen oxide removal there. The 10 purified offgas is discharged into the atmosphere. In place of the prior mixing of methane and ammonia, the gases can also be introduced separately into the gas containing nitrogen oxides before entry into the reactor.

15

Examples

The experiments described below were carried out in a laboratory set-up and illustrate the invention.

20

The catalyst employed was an iron-laden zeolite catalyst of the BEA type which was used as granules having a particle size of 0.7 - 1.4 mm.

25 As apparatus for reducing the N<sub>2</sub>O content in the examples below, use was made of a tube reactor which was charged with such an amount of the above catalyst, based on the inflowing gas stream, that a space velocity of 10 000 h<sup>-1</sup> resulted. The temperature of the 30 gas at the inlet of the reactor was set to 340°C by heating. Analysis of the gas stream entering and leaving the apparatus was carried out by means of an FTIR gas analyzer.

35 The composition of the gas mixture to be treated was:

1500 ppm of N<sub>2</sub>O; 600 ppm of NO<sub>x</sub>, 2.5% by volume of O<sub>2</sub>, 0.4% of H<sub>2</sub>O in N<sub>2</sub>.

Before the gas stream entered the catalyst bed, ammonia and methane or propane were added.

5 Depending on the amounts of reducing agents added, the following residual concentrations of N<sub>2</sub>O and NO<sub>x</sub> were obtained at the reactor outlet:

Example	Amount of NH <sub>3</sub> added	Amount of CH <sub>4</sub> added	Amount of C <sub>3</sub> H <sub>8</sub> added	Residual N <sub>2</sub> O concentration	Residual NO <sub>x</sub> concentration
1	700 ppm	450 ppm	-	897 ppm	16 ppm
2	800 ppm	450 ppm	-	25 ppm	0 ppm
3	500 ppm	-	500 ppm	425 ppm	26 ppm
4	600 ppm	-	500 ppm	129 ppm	2 ppm

10 As can be seen from the above table, a high degree of removal of N<sub>2</sub>O was achieved when the reduction of NO<sub>x</sub> by means of NH<sub>3</sub> addition is complete, as is the case in examples 2 and 4. Even low residual NO<sub>x</sub> concentrations, as shown in examples 1 and 3, inhibit the removal of  
15 N<sub>2</sub>O.

The process of the invention thus achieves high degrees of removal of N<sub>2</sub>O and NO<sub>x</sub> at low temperature. The invention is thus substantially superior to the prior  
20 art as disclosed in JP-A-90/00,884. This document reports degrees of removal of N<sub>2</sub>O of only about 60-80% at a significantly higher temperature of 450°C.